

²⁶~~26~~ 27. The process of claim ²⁵~~26~~, in which the amount of water used is between 0.3 and 1 liters per kilogram of hydrocarbon solvent used.

²⁷~~27~~ 28. The process of claim ¹⁶~~17~~, in which said stirring is carried out at a temperature between 0 and 70 °C.

^{B2}~~28~~ 29. The process of claim ²⁷~~28~~, in which said stirring is carried out at a temperature between 20 and 30 °C.

²⁹~~29~~ 30. The process of claim ¹⁶~~17~~, in which said phosphatidylserine is prepared by trans-phosphatidylation of phosphatidylcholines of natural or synthetic origin.

³⁰~~30~~ 31. The process of claim ¹⁶~~17~~, in which said serine portion is in L form.

REMARKS

Claims 1-4 and 6-16 were pending in the application (re-numbered 1-15 at the time of allowance). Claim 2 has been amended to alter the spelling of "xylene" to reflect English usage, and to introduce Markush group terminology. A marked-up version of the claim, showing the changes made, is presented in the Appendix. New claims 17-31 have been added. Claim 17 differs from claim 1 in that it recites "stirring" rather than "extraction". Support is found at page 3, lines 14-16 of the specification. Dependent claims 17-31 parallel claims 2-4 and 6-16, with minor differences as to form in the dependent claims. No new matter is introduced by the amendments. Upon entry of the amendment, claims 1-4 and 6-31 will be pending.

Respectfully submitted,
MORGAN & FINNEGAN, L.L.P.

Dated: November 19, 2002

By: James P. Demers

James P. Demers
Registration No. 34,320

Correspondence Address:

MORGAN & FINNEGAN, L.L.P.
345 Park Avenue
New York, NY 10154-0053
(212) 758-4800 Telephone

APPENDIX

Claim 2 as amended, showing changes made:

2. (*amended*) Process according to claim 1, in which said hydrocarbon solvent is [chosen among] selected from the group consisting of toluene, [xilene] xylene, n-heptane, n-hexane [or] and cyclohexane.